Appl. No. 10/611,496 Amdt. dated April 5, 2005 Reply to Office Action of March 22, 2005/December 2, 2004

This listing of claims replaces all prior versions, and listings of claims in the instant application:

## Listing of Claims:

1. (Original) An apparatus for separating a first gas from a mixture of the first gas and at least one second gas, the apparatus comprising:

a housing which comprises an inlet port and an outlet port;

an adsorbent which is positioned in the housing;
the adsorbent comprising a carbon based foam monolith that
has an affinity for the first gas;

wherein as the gas mixture flows through the housing, the first gas will be adsorbed onto the adsorbent and the second gas will exit the housing through the outlet port;

whereby the first gas is separated from the second gas.

- 2. (Original) The apparatus of claim 1, wherein the adsorbent comprises a thermal conductivity of at least 100 W/m-  $\rm K.$
- 3. (Original) The apparatus of claim 2, wherein the adsorbent comprises a thermal conductivity of at least about 150 W/m-K.
- 4. (Currently Amended) The apparatus of claim 1, wherein the adsorbent carbon based foam monolith comprises a mesophase pitch-based graphite foam product.

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- 5. (Currently Amended) The apparatus of claim 4, wherein the adsorbent mesophase pitch-based graphite foam product comprises a mesophase pitch-based activated graphite foam product.
- 6. (Original) The apparatus of claim 1, wherein the adsorbent comprises a number of gas flow passages extending therethrough.
- 7. (Original) The apparatus of claim 6, wherein the passages are aligned with at least one of the inlet and outlet ports.
- 8. (Original) The apparatus of claim 1, wherein the adsorbent comprises at least one cross sectional dimension which is smaller than a corresponding cross sectional dimension of the housing.
- 9. (Original) The apparatus of claim 8, wherein the adsorbent comprises two cross sectional dimensions which are each smaller than the corresponding cross sectional dimensions of the housing.
- 10. (Original) The apparatus of claim 9, wherein the adsorbent comprises means for supporting the adsorbent within the housing.

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11. (Original) The apparatus of claim 10, wherein the supporting means

comprises a number of elongated fins which are each aligned with at least one of the inlet and outlet ports.

- 12. (Original) The apparatus of claim 1, further comprising means for desorbing the first gas from the adsorbent.
- 13. (Original) The apparatus of claim 12, wherein the desorbing means comprises:
- a first electrical conductor which is positioned against a first surface of the adsorbent;
- a second electrical conductor which is positioned against a second surface of the adsorbent; and
- a power supply which is connected across the first and second conductors;

wherein upon activation of the power supply an electrical current is conducted across the adsorbent to desorb the first gas from the adsorbent in a desorption reaction.

- 14. (Original) The apparatus of claim 13, wherein the desorption reaction is substantially non-thermal.
- 15. (Original) The apparatus of claim 13, wherein the housing comprises the first and second conductors.

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- 16. (Original) The apparatus of claim 15, further comprising a number of cooling fins attached to at least one of the first and second conductors.
- 17. (Original) The apparatus of claim 12, wherein the desorbing means comprises a heater.
- 18. (Original) The apparatus of claim 17, wherein the heater comprises an electrical resistance heater.
- 19. (Original) The apparatus of claim 17, wherein the heater comprises a cylindrical outer diameter and the adsorbent comprises a generally circular cross section having an inner diameter which is approximately the same as the outer diameter of the heater.
- 20. (Original) The apparatus of claim 17, wherein the housing comprises an annular inner diameter and the adsorbent comprises a generally circular cross section having an outer diameter which is less than the inner diameter of the housing.
- 21. (Original) An apparatus for separating a first gas from a mixture of the first gas and at least one second gas, the apparatus comprising:
- a housing which comprises an inlet port and an outlet port;

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an adsorbent which is positioned in the housing; the adsorbent comprising a carbon based foam monolith that has an affinity for the first gas; and

means for desorbing the first gas from the adsorbent; wherein during a first phase of operation of the apparatus the first gas is adsorbed onto the adsorbent to separate the first gas from the second gas, and during a second phase of operation of the apparatus the first gas is

desorbed from the adsorbent and expelled through the outlet port.

- 22. (Original) The apparatus of claim 21, wherein the desorbing means comprises:
- a first electrical conductor which is positioned against a first surface of the adsorbent;
- a second electrical conductor which is
  positioned against a second surface of the adsorbent;
  and
- a power supply which is connected across the first and second conductors;

wherein upon activation of the power supply an electrical current is conducted across the adsorbent to desorb the first gas from the adsorbent in a desorption reaction.

- 23. (Original) The apparatus of claim 22, wherein the desorption reaction is substantially non-thermal.
- 24. (Original) The apparatus of claim 22, wherein the housing comprises the first and second conductors.

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- 25. (Original) The apparatus of claim 24, further comprising a number of cooling fins attached to at least one of the first and second conductors.
- 26. (Original) The apparatus of claim 21, wherein the desorbing means comprises a heater.
- 27. (Original) The apparatus of claim 26, wherein the heater comprises an electrical resistance heater.
- 28. (Original) The apparatus of claim 26, wherein the heater comprises a cylindrical outer diameter and the adsorbent comprises a generally circular cross section having an inner diameter which is approximately the same as the outer diameter of the heater.
- 29. (Original) The apparatus of claim 26, wherein the housing comprises an annular inner diameter and the adsorbent comprises a generally circular cross section having an outer diameter which is less than the inner diameter of the housing.
- 30. (Original) The apparatus of claim 21, wherein the adsorbent comprises a thermal conductivity of at least 100 W/m-K.

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- 31. (Original) The apparatus of claim 30, wherein the adsorbent comprises a thermal conductivity of at least about 150 W/m-K.
- 32. (Currently Amended) The apparatus of claim 21, wherein the adsorbent carbon based foam monolith comprises a mesophase pitch-based graphite foam product.
- 33. (Currently Amended) The apparatus of claim 32, wherein the adsorbent mesophase pitch-based graphite foam product comprises a mesophase pitch-based activated graphite foam product.
- 34. (Original) The apparatus of claim 21, wherein the adsorbent comprises a number of gas flow passages extending therethrough.
- 35. (Original) The apparatus of claim 34, wherein the passages are aligned with at least one of the inlet and outlet ports.
- 36. (Original) The apparatus of claim 21, wherein the adsorbent comprises at least one cross sectional dimension which is smaller than a corresponding cross sectional dimension of the housing.
- 37. (Original) The apparatus of claim 36, wherein the adsorbent comprises two cross sectional dimensions which are

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each smaller than the corresponding cross sectional dimensions of the housing.

- 38. (Original) The apparatus of claim 37, wherein the adsorbent comprises means for supporting the adsorbent within the housing.
- 39. (Original) The apparatus of claim 38, wherein the supporting means comprises a number of elongated fins which are each aligned with at least one of the inlet and outlet ports.
- 40. (Original) A method for separating a first gas from a mixture of the first gas and at least one second gas, the method comprising:

flowing the gas mixture over or through an adsorbent which has an affinity for the first gas; adsorbing the first gas onto the adsorbent; stopping the flow of the gas mixture; and desorbing the first gas from the adsorbent; wherein the adsorbent comprises a carbon based foam monolith.

- 41. (Original) The method of claim 40, wherein the adsorbent comprises a thermal conductivity of at least 100 W/m- $\rm K.$
- 42. (Original) The method of claim 41, wherein the adsorbent comprises a thermal conductivity of at least about 150 W/m-K.

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- 43. (Currently Amended) The apparatus of claim 40, wherein the adsorbent carbon based foam monolith comprises a mesophase pitch-based graphite foam product.
- 44. (Currently Amended) The apparatus of claim 43, wherein the adsorbent mesophase pitch-based graphite foam product comprises a mesophase pitch-based activated graphite foam product.
- 45. (Original) The method of claim 40, wherein the desorption step comprises using an electrical current to desorb the first gas from the adsorbent.
- 46. (Original) The method of claim 45, wherein the desorption step is substantially non-thermal.